

WASTEWATER FORMULA SHEET

$$\Pi (\text{pi}) = 3.1416$$

CIRCUMFERENCE OF CIRCLE = Π (Diameter)

SURFACE AREA:

Circle = Π (Radius)² = (1/4) Π (Diameter)² = 0.785 (Diameter) (Diameter)

Rectangle = (Length) (Width)

Triangle = (1/2) (Base) (Height)

VOLUME:

Circular Tank = Π (Radius)² (Height) = (1/4) Π (Diameter)² (Height)

Rectangular Tank = (Length) (Width) (Height)

Cone = (1/3) Π (Radius)² (Height)

TEMPERATURE CONVERSIONS:

$$F^{\circ} = (C^{\circ} + 17.78) (1.8)$$

$$C^{\circ} = (F^{\circ} - 32) (0.555)$$

ELECTRICAL:

Watts = (VOLTS) (AMPS)

Volts = (AMPS) (RESISTANCE)

$$1\text{Kw} - \text{hr} = 2.93 \times 10^{-4} \text{ BTU's}$$

MISCELLANEOUS CONVERSIONS:

$$1 \text{ Acre} = 43,560 \text{ Feet}^2$$

$$1 \text{ Feet}^3 = 7.48 \text{ Gallons}$$

$$1 \text{ Gallon (H}_2\text{O)} = 8.34 \text{ Pounds}$$

$$1 \text{ Meter}^3 = 35.3 \text{ Feet}^3$$

$$1 \text{ Gallon} = 3.78 \text{ Liters}$$

$$1 \text{ Pound} = 0.45 \text{ Kilograms}$$

Pounds (Lbs.)	= (flow MGD) (mg/l) (8.34 Lbs/Gal)
Detention Time (hrs)	= $\frac{(\text{Tank Vol. ft}^3) (7.48 \text{ gal/ft}^3) (24 \text{ hrs/day})}{\text{Flow (gal/day)}}$
Sludge Age (days)	= $\frac{(\text{MLSS mg/l}) (\text{Aeration Tank Vol. MG}) (8.34 \text{ lb/gal})}{(\text{Prim. Eff. SS mg/l}) (\text{Flow MGD}) (8.34 \text{ lb/gal})}$
Sludge Volume Index (ml/g)	= $\frac{(30 \text{ min. sett. solids in ml/l}) (1000)}{\text{MLSS (mg/l)}}$
Wasting Rate (MGD)	= $\frac{\text{Solids to be wasted in Lbs/day}}{(\text{RAS Conc. mg/l}) (8.34 \text{ lb/gal})}$
Wasting Rate (pounds)	= $\frac{(\text{Vol. of Aera. Tank in MG} + \text{Clarifiers in MG})}{(\text{Present MLSS} - \text{Desired MLSS}) (8.34 \text{ lb/gal})}$
MCRT (days)	= $\frac{(\text{Vol. of Aera. Tank} + \text{Clarifiers in MG}) (\text{MLVSS})}{[(\text{Flow in MGD}) (\text{Effluent VSS})] + \{(\text{WAS Flow}) (\text{Was VSS})\}}$
RAS Rate (% of Flow)	= $\frac{30 \text{ min settleability in ml.}}{(1000 \text{ ml.} - 30 \text{ min. settleability in ml.})}$
RAS Rate (MGD)	= $\frac{(\text{RAS Settleable Solids in ml/l}) (\text{Flow in MGD})}{(1000 \text{ ml/l} - \text{RAS Settleable Solids in ml/L})}$
Surface Loading Rate (gpd/ft ²)	= $\frac{\text{Flow in gpd}}{\text{Area in (ft.}^2\text{)}}$
Weir Overflow Rate (gpd/ft)	= $\frac{\text{Flow in gpd}}{\text{Weir Length in ft.}}$
B.O.D. (mg/l)	= $\frac{(\text{Initial D.O.} - \text{Final D.O.}) (300)}{\text{Sample in ml.}}$
B.O.D. (mg/l)	= $\frac{(\text{Initial D.O.} - \text{Final D.O.}) (100)}{\% \text{ Sample}}$
Suspended Solids (mg/l)	= $\frac{(\text{Wt.}_2 - \text{Wt.}_1) (1,000,000)}{\text{Sample Size in ml.}}$
Efficiency (%)	= $\frac{(\text{Value IN} - \text{Value OUT}) (100)}{\text{Value IN}}$
Reduction of Volatile Matter (%)	= $\frac{(\text{Value IN} - \text{Value OUT}) (100)}{(\text{Value IN} - [(\text{Value IN})(\text{Value OUT})]}$
$\frac{\text{FOOD MASS}}{\text{LBS of Available Biomass}} = \frac{\text{LBS of Incoming "food"}}{\text{LBS of Available Biomass}}$	= $\frac{(\text{Flow MGD}) (\text{Aera. Tank Influent BOD in mg/l})(8.34\text{lb/gal})}{(\text{MLVSS}) (\text{Aera. Tank Volume in MG}) (8.34 \text{ lb.gal})}$